







DESIGN, FABRICATION AND CONSTRUCTION ISSUES ASSOCIATED WITH AMMONIA STORAGE AT VARIOUS SCALES

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#### AGENDA AND PRESENTATION OUTLINE

- Introduction
- · Codes and Standards
- Storage Concepts
- · Ammonia Storage Tank Safety Considerations: Pressure, Vacuum and Level management
- Miscellaneous Safety System

<u>Acknowledgement:</u> This presentation is put together by the members of Matrix PDM Engineering – Project Engineering, Shell & Plate and Process Engineering Teams



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   One of the largest & most modern heavy steel plate fabricating facilities in the U.S.
- · ORANGE, CA

#### **PIPE SPOOLING & MODULES**

- · BELLINGHAM, WA
- · LEDUC, AB



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#### **ENERGY**

- Storage terminals
- Refineries
- Gas processing plants
- Petrochemical plants
- Compressor stations
- LNG liquifaction and regassification plants
- Peak shaving facilities
- LPG export facilities
- Renewables

#### **POWER**

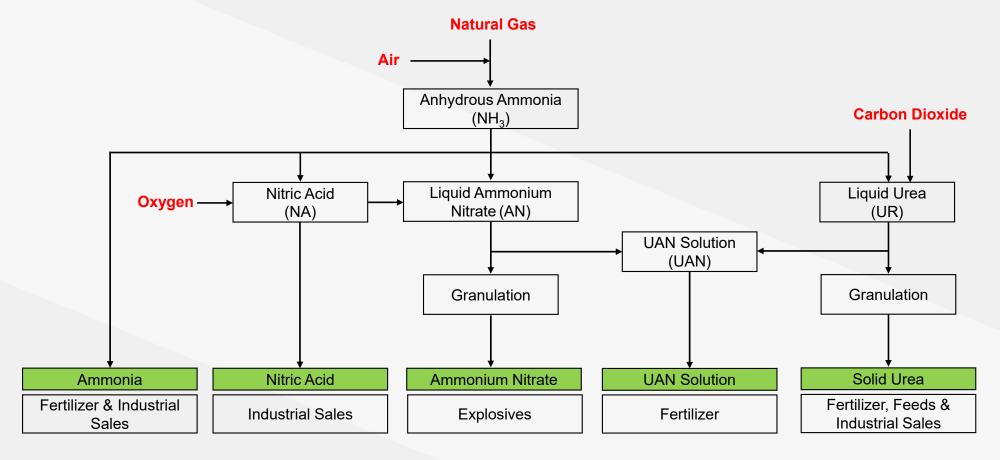
- Substations
- Transmission and distribution
- Combined-cycle power plants
- Nuclear plants
- Storm response

#### **INDUSTRIAL**

- · Iron and steel mills
- Fertilizer plants
- · Cement facilities
- Manufacturing plants
- Mining and minerals

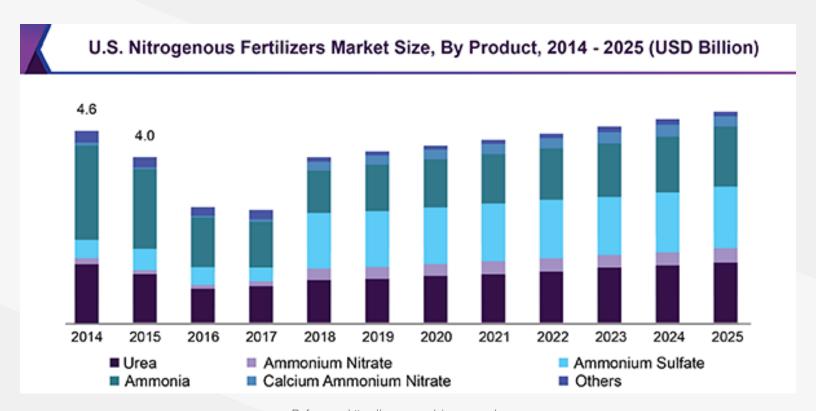


# AMMONIA, A BASIC BUILDING BLOCK FOR NITROGENEOUS FERTILIZERS





### FERTILIZER MARKET



Reference: https://www.grandviewresearch.com



# AMMONIA PROPERTIES

| Physical Properties of Ammonia                      |                           |  |
|---|---------------------------|--|
| Molecular Weight                                    | 17.03 g/mol               |  |
| Saturation Temperature / Boiling Point at 14.7 psia | -28 °F                    |  |
| Freezing Point at 14.7 psia                         | -107.9 °F                 |  |
| Saturated Liquid Density at 14.7 psia               | 42.57 lb/ft <sup>3</sup>  |  |
| Saturated Vapor Density at 14.7 psia                | 0.0555 lb/ft <sup>3</sup> |  |
| Critical Pressure                                   | 1657 psia                 |  |
| Critical Temperature                                | 271.4 °F                  |  |
| Flammability Limits (%in air, by volume)            | 16% to 25%                |  |
| Ignition Temperature                                | 1562 °F                   |  |
| Latent Heat of Vaporization                         | 589.3 Btu/lb              |  |



## AMMONIA - A CHEMICAL THAT NEEDS SAFE HANDLING

| Concentration / Time             | Effect   |
|----------------------------------|--|
| 20 ppm – 50 ppm                  | Mild discomfort, depending on whether an individual is accustomed to smelling ammonia      |
| 50 ppm (OSHA Max exposure limit) | Perceptible eye and throat irritation  |
| 100 ppm for 2 hours              | Nuisance eye and throat irritation   |
| 134 ppm for 5 minutes            | Tearing of the eyes, eye irritation, nasal irritation, throat irritation, chest irritation |
| 140 ppm for 2 hours              | Severe irritation, need to leave exposure area   |
| 300 ppm - 500 ppm for 30 minutes | Upper respiratory tract irritation; tearing of the eyes (lacrimation), hyperventilation    |
| 700 ppm – 1700 ppm               | Incapacitation from tearing of the eyes and coughing                                       |
| 5000 ppm – 10,000 ppm            | Rapidly fatal  |
| 10,000 ppm                       | Promptly lethal  |

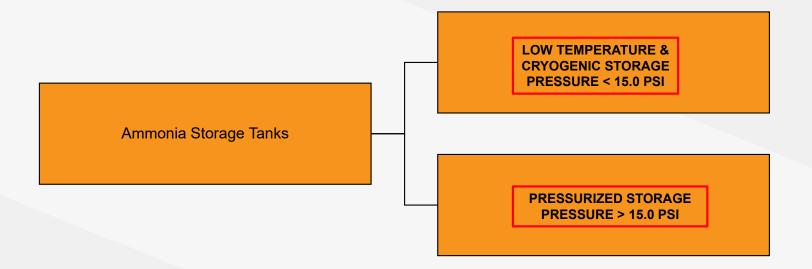
MATRIX PDM ENGINEERING

# AMMONIA FACILITES STANDARDS

| Reference              | Description  |
|------------------------|--|
| 29 CFR § 1910.119      | Process safety management of highly hazardous material:          |
| 6 CFR Part 27          | Chemical Facility Anti-Terrorism Standards (CFATS)               |
| 29 CFR 1910.111 (OSHA) | Storage and handling of anhydrous ammonia                        |
| 49 CFR Parts 171-180   | Transportation of Hazardous Materials                            |
| 33 CFR 105             | Maritime Security of Facilities                                  |
| US-EPA EPCRA           | Emergency Community Right-to-know Act                            |
| US-EPA RMP             | Risk Management Plan   |
| General Considerations | Quantitative Risk Assessment; Equipment Layout - Ammonia         |
|                        | Process Area; Ammonia Process Storage Area; Transportation Send- |
|                        | out Area; Plant Operations and Maintenance; Emergency Response;  |
|                        | Natural events – Hurricanes, Flooding, and Earthquake            |

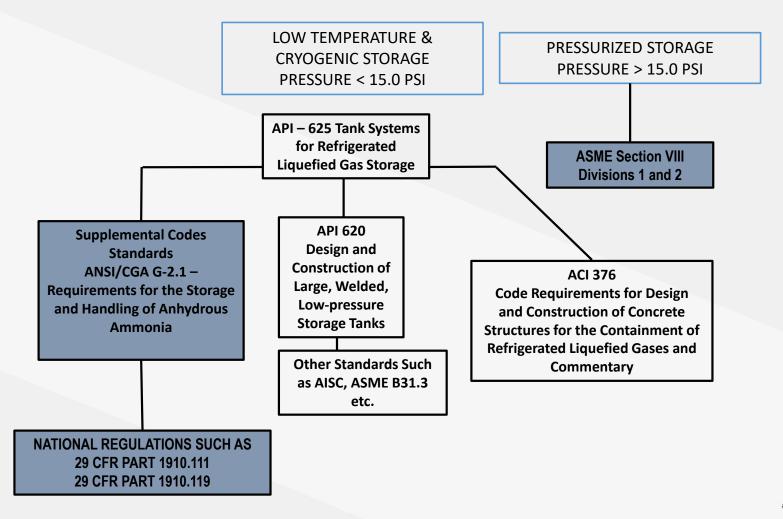


## METHODS TO STORE AMMONIA



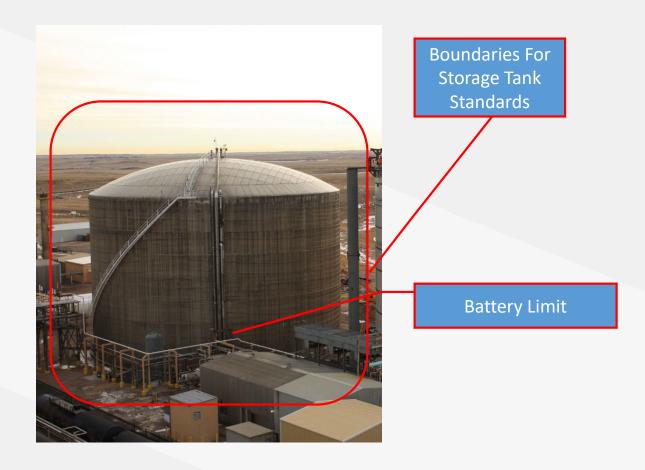


#### TYPICAL U.S. STORAGE CODES AND STANDARDS





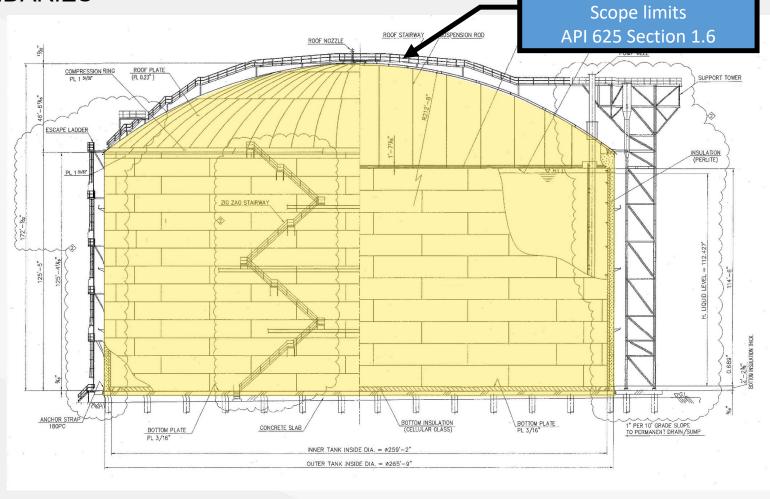
# **BOUNDARIES**





CODES AND STANDARD

## **BOUNDARIES**





# AMMONIA, STORAGE TANKS



Reference: Iowa Fertilizer Plant, Weaver, Iowa, USA



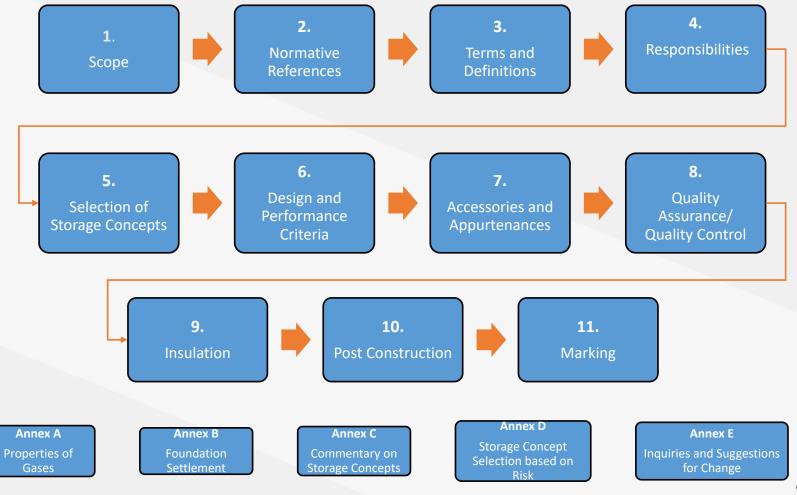
## AMMONIA STORAGE – DESIGN PARAMETERS

| Description                    | Value  |
|--------------------------------|--|
| Storage Tank Gross<br>Capacity | 5,000 MT to 50,000 MT (Can go to 70,000 MT or higher.) |
| Design Pressure                | 1.0 psig to 4.0 psig (Typ. 2.0 psig)                   |
| Design Temperature             | -35 deg. F   |



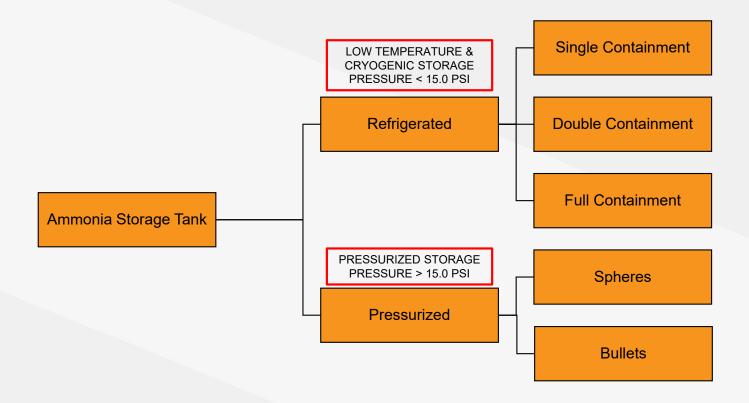


#### API 625 STRUCTURE - STORAGE TANK SYSTEM



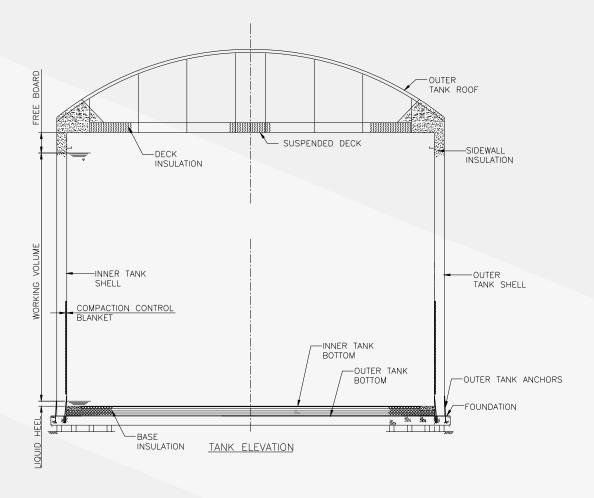


## METHODS TO STORE AMMONIA





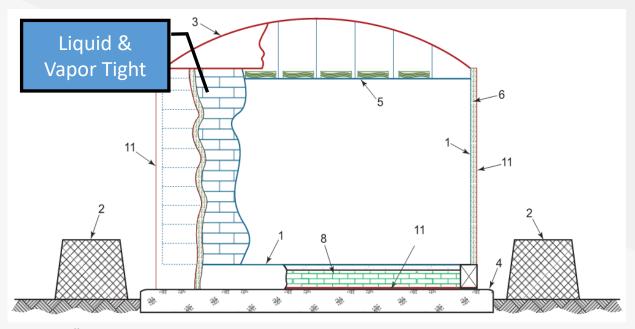
## NOMENCLATURE – BASIC CRYOGENIC STORAGE TANK





14 ring beam

# SINGLE CONTAINMENT TANK SYSTEM (API 625, SECTION 5.2 & ANNEX C.2)



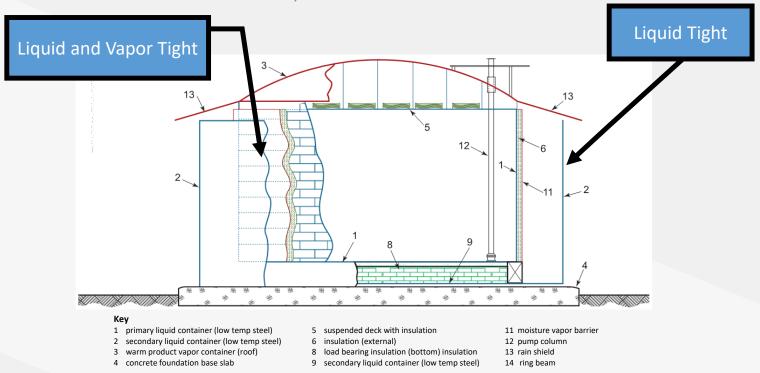
#### Key

- 1 primary liquid container (low temp steel)
- 2 secondary containment (dike wall)
- 3 warm product vapor container (roof)
- 4 concrete foundation

- 5 suspended deck with insulation
- 6 insulation (external)
- 8 load bearing insulation (bottom)
- 11 moisture vapor barrier
- Normal Operating Condition: # Primary: liquid and vapor tight
- Emergency Operating Condition: Dike will retain the liquid



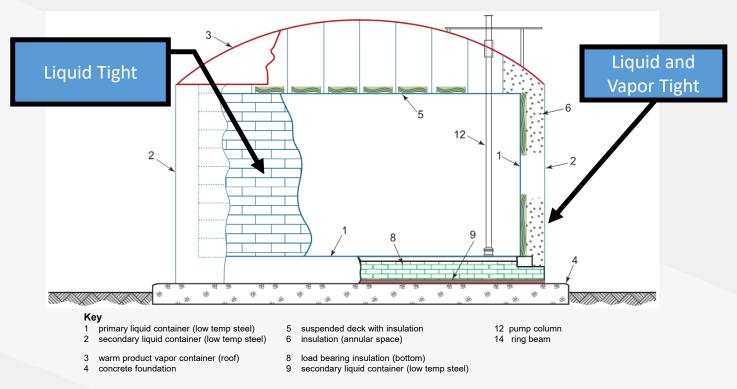
# DOUBLE CONTAINMENT TANK SYSTEM, STEEL DIKE (API 625, SECTION 5.3 AND ANNEX C.3)



- Normal Operating Condition: # Primary: liquid and vapor tight # Secondary: liquid tight
- Emergency Operating Condition: Secondary will retain the liquid



# FULL CONTAINMENT TANK SYSTEM, STEEL (API 625, SECTION 5.4 & ANNEX C.4)



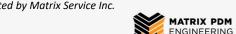
- Normal Operating Condition: # Primary: liquid and vapor tight # Secondary: liquid tight
- Emergency Operating Condition: Secondary will retain the liquid

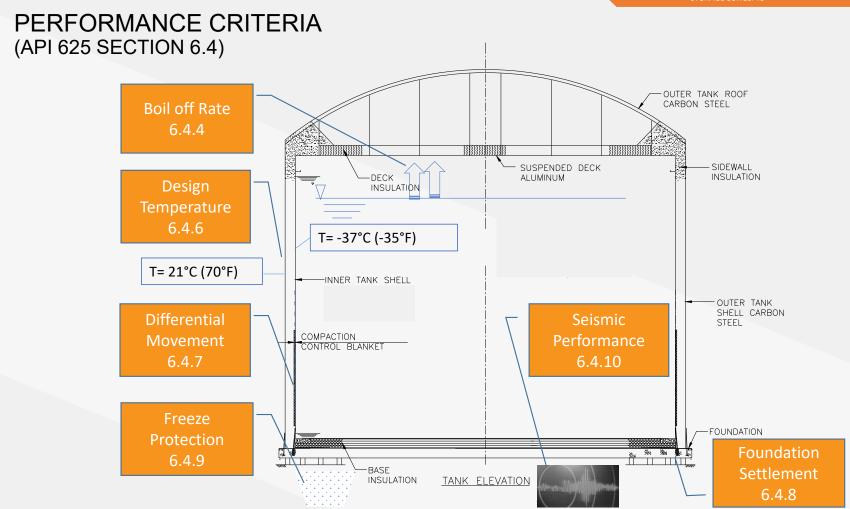


## **FULL CONTAINMENT STEEL TANKS**



Two 74,000 m<sup>3</sup> Ammonia Tanks – Orascom – Wever, IA







# FOUNDATIONS (PILE CAP REBAR CAGE)





# FOUNDATION HEATING SYSTEM





# AMMONIA STRESS CORROSION CRACKING (NH3-SCC)

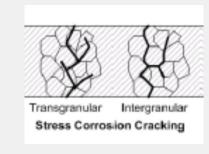
- NH3-SCC affects mechanical integrity
- Oxygen + Stress enables SCC
- SCC is less prevalent in low temperature storage tanks

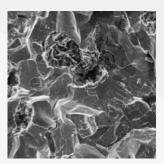
#### **Prevention**

- · Design, fabrication and construction details
- Minimization of oxygen contamination during commissioning and operation
- Providing a small amount of moisture (0.2%) during operation

#### **Inspection**

- Wet Magnetic Particle Testing
- UT Testing (Shear Wave + TOFD)
- Acoustic Emissions









Intergranular Fracture

#### Reference

Dettmers, Reindell; Stress Corrosion Cracking Update, Presentation, www.irc.wisc.edu

Nyborg, Lunde; Measures for Reducing SCC Anhydrous Ammonia Storage Tanks, AlChE, Aiche-35-005, 1994

Mortenson; In-service inspection of welds in atmospheric ammonia storage tanks, https://www.semfa.eu/Portals/6/Presentations/Inspection%20of%20Ammonia%20Storage%20Tanks



#### LOW TEMPERATURE STORAGE TANKS WITH SIDE PENETRATIONS

Double or Full Containment Tanks with Side or bottom penetrations are allowed if:

- Purchaser specifies the penetrations
- Regulations do not prohibit them
- Risk assessment considers the penetrations
- In-tank valves are provided
- A remote dike wall is provided in addition to the secondary containment. The volume contained by the dike shall be equal to 110 % of the flow from a full line break prior to closure of the intank valve.





### STORAGE TANKS WITH IN-TANK VALVES

#### Requirements

- Automatic activation failure of external piping
- Automatic activation loss of electrical power
- Activation from a remote location.
- Failure of the penetrating nozzle resulting from external pipe strain is beyond the shutoff seats of the internal valve.



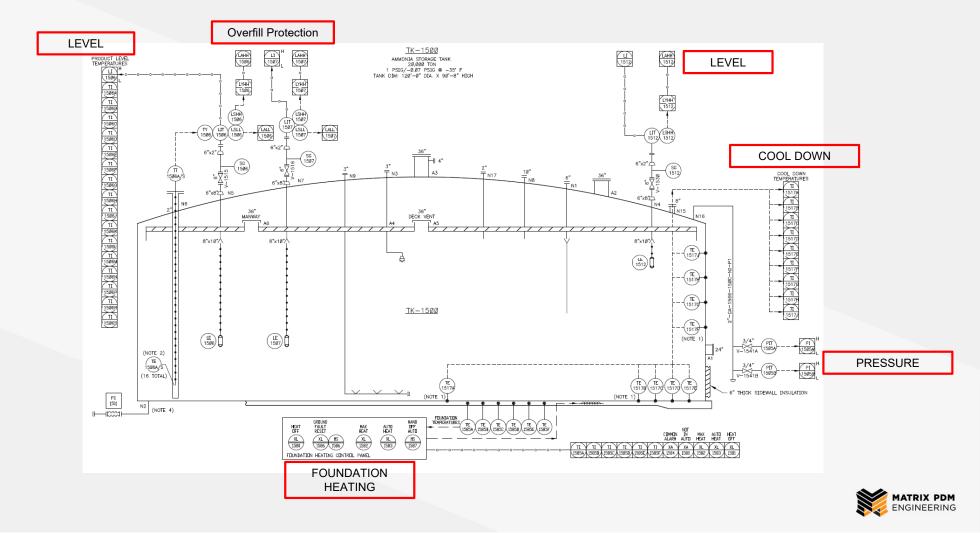


#### AMMONIA REFRIGERATED STORAGE TANK KEY SAFETY CONSIDERATIONS

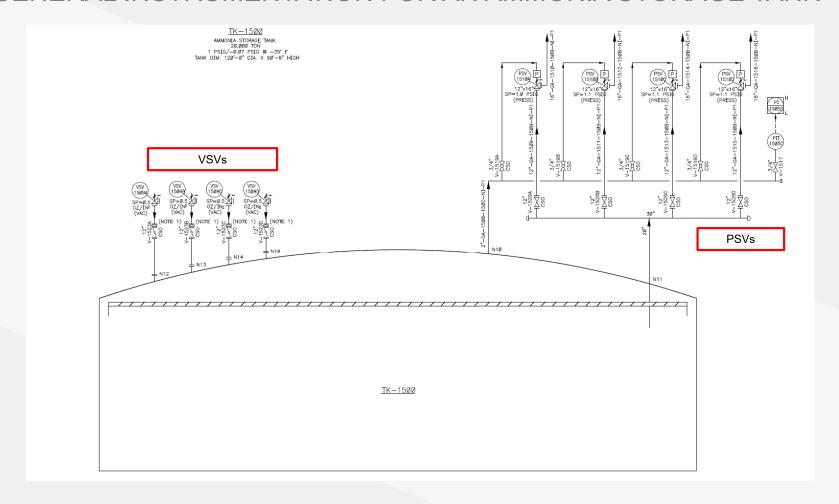
- Pressure Management
- Vacuum Management
- Level Management



### GENERAL INSTRUMENTATION FOR AN AMMONIA STORAGE TANK



## GENERAL INSTRUMENTATION FOR AN AMMONIA STORAGE TANK





## CAUSE OF TANK HIGH PRESSURE

- Tank Heat Gain
- Fill Flash
- · Vapor Displacement due to Liquid Filling
- Decrease in Barometric Pressure
- Heat Input from Pump Recirculation
- Abnormal Operating Conditions
- Fire Exposure
- Leakage through Inner Tank





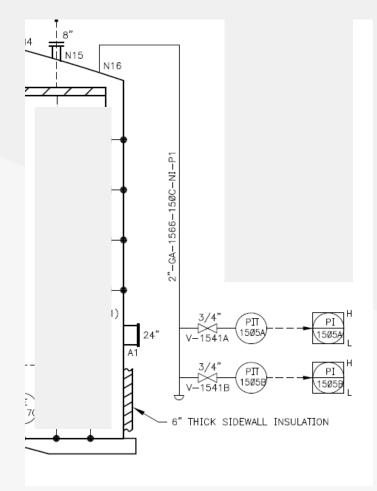
Reference: The Rupture of a Liquid Ammonia Storage Tank Study, Alireza Orooji and Sajjad Hosseininia, Assaluyeh, Iran



## TANK PRESSURE MEASUREMENT

#### **Pressure Gauge**

- Minimum two pressure instruments are required
- Pressure instruments shall be connected to the vapor space above liquid level





Pressure Management

Condensing System

1st line of defense

Pressure Safety Valve

3rd Line of Defense



#### **Condensing System / Vapor**

#### Recovery

Design parameters

· Fill Displacement

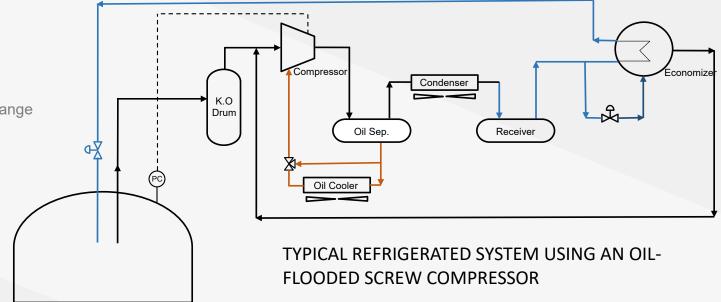
Fill Flash

Tank Heat Gain

• Recirculation Heat Gain

• Barometric Pressure Change

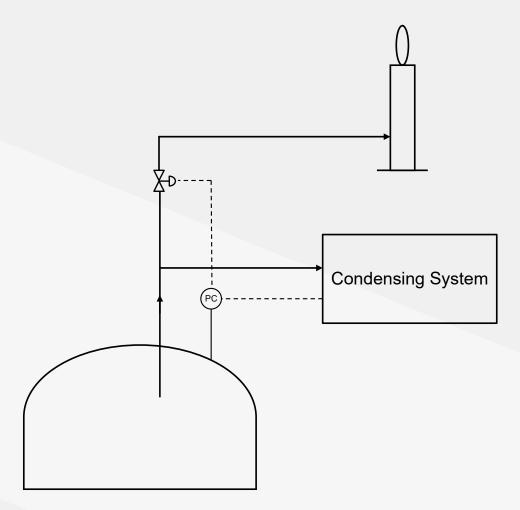
Set pressure





#### Flare

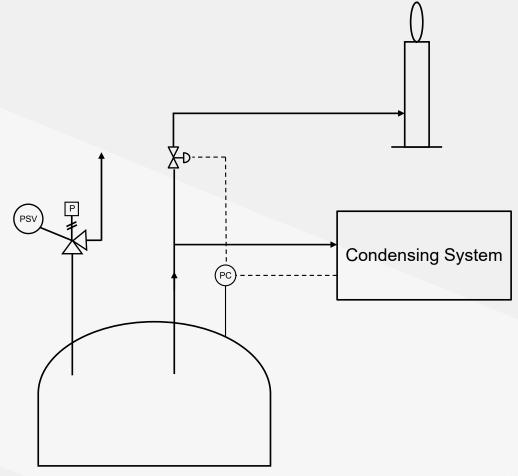
- As a Back up for Condensing System
- Design parameters
  - Fill Displacement
  - Fill Flash
  - Tank Heat Gain
  - Recirculation Heat Gain
  - Barometric Pressure Change
- Set pressure





#### **Pressure Safety Valves**

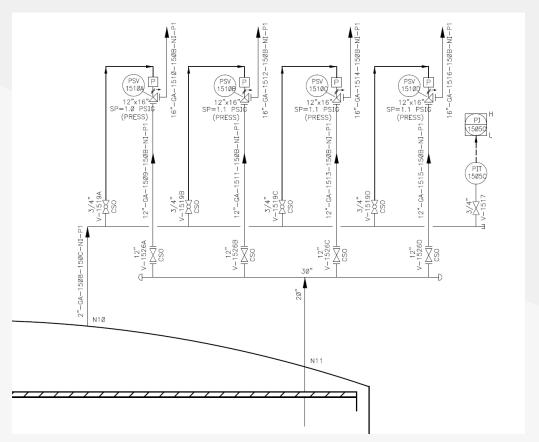
- Design parameters
  - Normal Operating Conditions
  - Fill Displacement
  - Fill Flash
  - Tank Heat Gain
  - · Recirculation Heat Gain
  - Barometric Pressure Change





#### **Pressure Safety Valves**

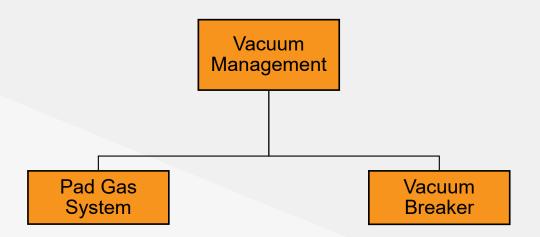
- Design parameters
  - Abnormal Operating Conditions
  - Fire Exposure
  - · Utility or Mechanical failure
- Excessive pumping rates into the tank
- Excessive temperature of ammonia liquid pumped into the tank below the liquid level
- Leakage through Inner Tank and Overfill (Full Containment Tank Only)
- Set Pressure





## CAUSE OF TANK LOW PRESSURE

- Withdrawal of Liquid
- Withdrawal of Vapor
- Increase in Barometric Pressure
- Abnormal Operating Conditions

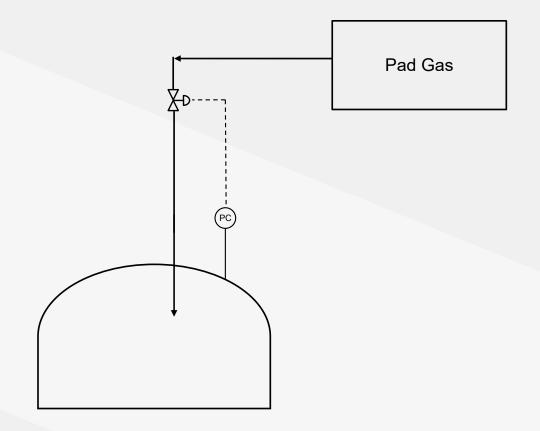




## **VACUUM MANAGEMENT**

#### **Pad Gas System**

- Design parameters
  - Liquid Withdrawal
  - Vapor Withdrawal
- Set pressure

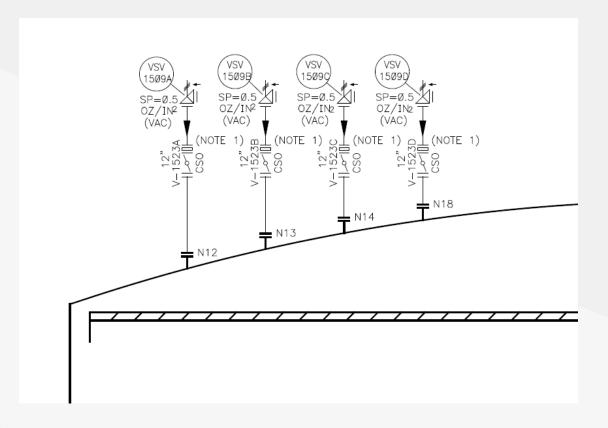




## **VACUUM MANAGEMENT**

#### **Vacuum Breakers**

- Design parameters
  - Normal Operating Conditions
  - Liquid Withdrawal
  - Vapor Withdrawal
  - Barometric Pressure Change
  - Abnormal Operating Conditions
  - Utility or Mechanical Failure
  - Excessive Withdrawal Rates
  - Set pressure





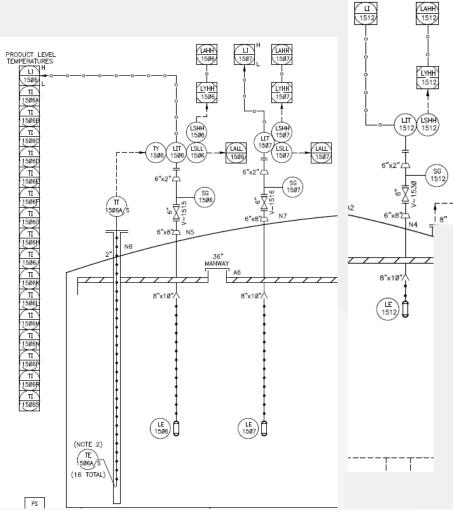
#### LEVEL MANAGEMENT

#### **Level Gauges and Overfill Protection**

- Minimum two independent level gauges
- A separate, liquid level alarm and cutoff device, set at the design liquid level
- Overfill protection margin

#### Leak detection

- A must for a double and full containment tanks, required for single containment tanks only if specified by the owner or by a result of a hazard study
  - Temperature Change
  - Gas Detection
  - Level (Differential pressure measurement)





## MISCELLANEOUS SAFETY SYSTEMS

#### **Hazard Detection**

- Gas Detectors
- Flame Detectors
- Smoke Detectors
- Horns and Beacons
- Hand Switch Stations
- Fire System















#### SUMMARY

- · Ammonia is a toxic chemical that requires safe handling
- Ammonia Tanks are built using low pressure welded storage tank standards
- Storage Tanks for Refrigerated Liquids are considered a System with many components
- Primary Safety Considerations for Large Scale Ammonia Storage are Pressure, Vacuum and Level management
- These aspects are managed using Instrumentation
- · Matrix has a proven track record in the design, fabrication and construction of ammonia tanks at various scales





# **THANK YOU**

